PRELIMINARY ENGINEERING REPORT FOR:

# TOWN OF EDISTO BEACH, SC WATER SYSTEM IMPROVEMENTS

PREPARED FOR: TOWN OF EDISTO BEACH, SC

J-25683.0000



o. 186

Prepared by:

THOMAS & HUTTON

www.thomasandhutton.com

### TABLE OF CONTENTS

. IntroductionPag	je 1
. General InformationPag	je 1
. Service Area & Existing Water SystemPag	je 2
. Proposed ProjectPag	je 5
. Water DemandPag	je 7
. Supply & Transmission LinePag	je 7
. TreatmentPage	e 10
. StoragePage	e 15
. Control SystemPage	e 15
0. Hydraulic ModelPage	e 19
1. SummaryPage	e 21

### FIGURES:

Location Map
Water System Map
Water System Improvements Map4.1
Proposed Well Diagram
RO Treatment Plant-Floor Plan7.1
RO Treatment Plant-Elevation Section7.2
RO Treatment Plant & Well #7 Site Plan7.3
Process & Instrumentation Diagrams9.1
Process Flow Diagram
Hydraulic Modeling Graph – Option 4C10.1

### TABLES

Summary of Existing Potable Supply Wells	3.1
Total Average Well Production	5.1
Proposed Potable Supply Wells	6.1
Summary of RO Plant Flow Rates	7.1
Water Quality Projections	7.2

### CHARTS

sto Beach-2015 Water Use
--------------------------

### **APPENDICES:**

Lab Analysis – Existing Well #6	Appendix A
Reverse Osmosis System Analysis	Appendix B

### 1. INTRODUCTION

The existing water system is in full compliance with primary regulations but is noncompliant with current Fluoride secondary standards. Also, because the water system has other significant issues with taste and corrosiveness, the Town of Edisto Beach has voted to proceed with major improvements to the water system which will correct any deficiencies and quality concerns currently identified. This Preliminary Engineering Report (PER) will describe specific water system improvements proposed to meet these goals set by Town Council:

- A. Improve water quality.
- B. Increase ability of the system to meet peak daily demand (PDD).
- C. Design for projected demand of 20% above current average daily demand (ADD).
- D. Utilize existing system components to the fullest extent possible.

### 2. <u>GENERAL INFORMATION</u>

Α.	DHEC System ID Number:		15WS002
в.	DHEC Operating Permit Number:		SC1510006
C.	Responsible O Name & Title:	fficial, Town of Edisto B Jane Darby, Mayor	each, SC
	Address:	2414 Murray Street Edisto Beach, SC 2943	8
	Phone:	(843) 869-2505	
D.	Director of Pub Name & Title:	to Beach, SC reatment License, Class "A" Distribution	
	Address:	2414 Murray Street Edisto Beach, SC 2943	8
	Phone:	(843) 869-2505	
E.	Engineer Name:	Thomas & Hutton Eng	ineering Co.
	Address:	682 Johnnie Dodds Bl Mt. Pleasant, SC 2946	vd., Suite 100 4
	Phone:	(843) 849-0200	

Engineer: Mark F. Yodice, P.E., No. SC 13293



### 3. <u>SERVICE AREA & EXISTING WATER SYSTEM</u>

The Town of Edisto Beach is located at the end of Hwy. 174 approximately 20 miles south of Hwy. 17 as shown on **Figure 3.1**. Edisto Beach consists of the island bounded by the Atlantic Ocean, Edisto River and Big Bay Creek as shown on **Figure 3.2**. The Edisto Beach water system service area includes the area within the Town limits and it also serves the Edisto State Park and businesses along Hwy. 174 up to Palmetto Rd. including the True Value Hardware Store shopping complex located near this intersection. All areas north of Palmetto Rd. are located in Charleston County and are therefore not served. A large portion of the economy is based upon tourism. The terrain is flat and soils are sandy with a high groundwater table, especially at high tide.

There are currently 641 permanent residents but there are 2,360 water customers due to the resort nature of this community. Most customers are single family residential with a mixture of condominiums and commercial. A large portion of the residential units are rentals for visitors especially during the summer months. There are 2185 residential customers (92.6%) and 175 commercial customers (7.4%). Meters are read on a 6-month basis to coincide with the billing cycle.

**Figure 3.2** indicates the location of components that comprise the existing public water supply including; six active wells, 100,000-gallon elevated storage tank (ET), 200,000-gallon ground storage tank (GST) with booster pumps and a water distribution system. Four of the six active wells pump directly into the distribution system after being treated with only chlorination (sodium hypochlorite). The two remaining wells are located off-island in Edisto State Park and they pump directly into the 200,000-gallon GST after receiving chlorination and they are controlled by water level in the GST. The two boosters deliver water from the GST to the distribution system at an average pumping rate of 500 gpm, and they are driven with VFD motors. The boosters are controlled by water level in the elevated tank. A summary of the existing well characteristics is presented in Table 3.1.

TABLE 3.1       Town of Edisto Beach								
	Sum	mary of Ex	isting Pota	ble Supply \	Nells			
Well No.	Location	Depth	(feet)	<b>Casing Size</b>	Year	Capacity		
		Bore Hole Casing		(inches)	Completed	(gpm)		
#1	Dockside	555	539	8	1979	250		
#2	Bay Point	552 346		6	1962	135		
#3	Lions Club	565 540		4	1975	90		
#4	Edisto Park	562 534		6	1973	186		
#5	Edisto Park	593 532		8	1993	276		
#6	McConkey	580	540	8	2000	495		

URS RO/ASR Feasibility Study 2012

February, 2017

Figure 3.1

Location Map





February, 2017

Figure 3.2

Water System Map





### 4. <u>PROPOSED PROJECT</u>

The Town developed an intensive program for the selection of a Progressive Design/Build team to complete the water system's improvements. The team selected for this project includes:

- Wharton-Smith, Inc., Sanford, FL, General Contractor
- Harn RO Systems, Inc., Venice, FL, RO Equipment Manufacturer
- Thomas & Hutton, Mt. Pleasant, SC, Design/Permitting Engineer

The team developed eight various options with associated costs and presented this to the Town in a matrix format during Phase 1 of the project. The options consisted of combinations including; Middendorf or Santee well supply, aquifer storage and recovery (ASR) or clearwell storage, various sizes of reverse osmosis (RO) treatment plants, two different locations for the RO plant and concentrate discharge lines, use of existing GST during peak demand season. The team provided budget pricing and prepared a hydraulic model for each option to compare their ability to meet PDD with fire flow. The Town selected Option 4C consisting of the improvements as shown on **Figure 4.1** and more fully described in the following sections.

Phase 1 of this Progressive Design/Build also includes completion of this PER and sufficient design detail to allow the team to present a Guaranteed Maximum Price (GMP) for the complete project to the Town. Phase 2 will not begin until the Town accepts the GMP and authorizes the team to proceed and it will consist of completion of construction drawings, procurement of required permits, construction, and commissioning of the project.

February, 2017

Figure 4.1

Water System Improvements Map





### 5. <u>WATER DEMAND</u>

With direction from the Town, the team utilized previous engineering studies and historical water use records to develop the projected water demand for design purposes. Previous studies concluded that the average daily water demand per customer was 250 gallons per day (gpd). Current customer base is 2,350; therefore, current average daily demand (ADD) is 587,500 gpd. Table 5.1 is a table of well-pumping records over a 6-year period as reported to SCDHEC which indicates an average usage of 530,720 gpd over that period of time.

The current ADD of 587,500 gpd should be conservative since water usage has been declining over recent years and the service area is approximately 87% built out. The Town requested that projections for future demand should be limited to 20% more than current usage; therefore, the design ADD will be 705,000 gpd (587,500 gpd X 1.2).

TABLE 5.1										
Total Average Well Production (gpd)										
Well #	Well #         2010         2011         2012         2013         2014         2015									
1	53,351	46,800	49,660	60,236	56,041	51,142				
2	40,112	45,263	46,164	43,504	39,748	51,214				
3	31,712	32,479	24,615	26,819	31,901	21,096				
4	85,200	89,068	50,951	70,205	53,082	40,504				
5	150,819	166,329	189,900	163,151	156,025	125,526				
6	229,855	208,055	228,890	147,559	147,890	129,444				
ADD (gpd)	591,049	587,995	590,180	511,474	484,688	418,926				
Peak Day		1,410,300	1,263,800	1,095,600	1,244,300					
Peak Factor		2.40	2.14	2.14	2.57					

Well records also indicate that the peak daily demand (PDD) factor has ranged between 2.14 to 2.57. A peaking factor of 2.30 was chosen for design purposes which yields a PDD of 1,621,500 gpd (1.622 mgd) or 1,126 gpm.

### 6. <u>SUPPLY & TRANSMISSION LINE</u>

The goal of this project is to supply only water treated by the RO plant at all times so the supply wells will be piped directly to the RO plant. Total well capacity to the plant will be 1,521 gpm consisting of three existing wells and two new wells drilled into the Santee aquifer. Although it is not possible to predict the exact capacity of the proposed wells, each will be 10-inch diameter designed to accommodate a submersible pump and motor with a capacity of at least 507 gpm each.

The system must be carefully monitored to ensure that current groundwater withdrawal limits are not exceeded. Annual withdrawal permit currently allows 256 MG/year to be withdrawn from the aquifer or an average of 701,370 gpd. The proposed RO system will produce 553,713 gpd based upon this withdrawal limit. Assuming a 2% increase in water



use annually and the 2015 system usage average of 418,926 gpd, this withdrawal limit will be reached in the year 2029. A January 9, 2017 letter from DHEC recommends: "if increased usage indicates that the permitted withdrawal amount needs to be increased, the Department will gladly review a request for an increase at that time".

This first new well (Well #7) will be located on the site of the proposed RO plant as indicated on **Figure 7.3**. The location of the second new well is yet to be determined but it will most likely be located near the plant yet at a distance to minimize interference with the first well. The Town is currently negotiating for ownership of "Tract M" as shown on **Figure 4.1** and may select this site as the location of the second new well (Well #8). However, for purposes of this report it will be assumed that the second new well will be located at the site of existing Well #3 and will be labeled "New Well #3A" as indicated on **Figure 4.1**.

Existing wells #1, 2, and 6 will be connected to the RO plant with a dedicated transmission line as indicated on **Figure 4.1**. Chlorination of these wells will be discontinued since the RO plant will be designed to treat raw well water with post chemical addition including chlorination. All wells will have variable frequency drive (VFD) motors controlled by a new SCADA system. The remainder of the existing wells will be removed from the distribution system upon completion of the improvements, but will remain on standby status for emergency use only. Table 6.1 lists the existing and proposed wells that will provide the supply to the proposed RO Plant. Well #6 will be upgraded to 510 gpm.

All wells connected to the RO plant must be flushed to reduce the silt density index (SDI) for a period of time prior to discharging into the transmission line to the plant. An automatic valve will be installed on the discharge piping of each well. The valves will be controlled by SCADA based upon the flushing time required for each well. The flush water will be discharged into nearby drainage systems.

The new wells will be constructed as shown on the typical well diagram **Figure 6.1**. The wells will be completed with submersible pumps and motors with the well casing fitted with a blind flange to protect against the 100-year flood. VFD motors will allow the pumps to deliver 510-750 gpm. All piping extending through the well casing will be installed with welded fittings including the discharge piping, power cord conduit, airline conduit, and vent pipe. The vent pipe will be extended to an elevation of 1 foot above the 100-year flood elevation. All electrical switch gear and controls will be housed in pedestal-mounted NEMA 6X stainless steel panels. Each of the new wells will be designed and constructed in accordance with SCDHEC regulations unless waivers are granted.

J-25683.0000

February, 2017

TABLE 6.1         Town of Edisto Beach								
		Proposed F	Potable S	upply Wells				
Well No.	Location	Depth (f	Depth (feet) Casing Size Year Capacity					
		Bore Hole Casing (inches) Completed (gpm)						
#1	Dockside	555	539	8	1979	250		
#2	Bay Point	552 346 6 1962 13				135		
#6	McConkey	580	540	8	2000	495		
#7	RO Plant	600 540 10 2017 510				510		
#8	TBD	600	540	10	2017	510		



February, 2017

Figure 6.1

Proposed Well Diagram





### 7. <u>TREATMENT</u>

The proposed RO plant will be located on Town-owned property located on the south side of Murray St. (Lee St.) between Holmes and Loring Streets as shown on **Figure 4.1** with dimensions of 75 feet X 308 feet. The property is zoned PB which allows water treatment facilities. This site will not be adequate for future plant expansion; however, the Town feels plant capacity will be sufficient through buildout. The 100-year flood elevation at this location is 15 feet above MSL in a VE zone according to FEMA; however, the latest draft of the FEMA map indicates this location is in an AE zone with the 100-year flood elevation of 9 feet above MSL. Ground elevation at this location averages from 6 to 7 feet above MSL.

The operating floor of the treatment plant will be elevated to at least 2 feet above the 100-year flood elevation, as it will be supported by a reinforced concrete clearwell with an 11-foot water depth.

Treatment units will consist of three RO trains rated at 320 gpm permeate per train for a total permeate production 960 gpm. The system will be designed for 75% recovery and 20% raw water blend. Scale inhibitor will be added prior to the cartridge filters. The blended product water; therefore, will be 1,200 gpm total for all trains or a 24-hour production rate of 1.728 million gallons per day (mgd). The blended water will be further treated after the RO and blending processes by addition of calcium chloride for stabilization and sodium hypochlorite for disinfection before discharging into the clearwell. These chemicals will be housed in a separate room located within the treatment plant building. Three high service pumps (HSP) will deliver the finished water from the clearwell into the distribution system. The pumps will be located at the opposite end of the clearwell from the discharge point of the treated water. These pumps will be vertical turbine pumps with VFDs; one will be rated at 1,200 gpm while the other two will be rated at 600 gpm each. Concentrate from the RO process will be piped from the plant to the Atlantic Ocean along Loring Street as shown on Figure 4.1. Concentrate flow rate from each train will be 106.64 gpm for a total flow rate of 320 gpm when the plant is operating at full capacity. The concentrate line will be installed by horizontal directional drilling (HDD) under the dunes and ocean floor to the discharge point where a diffuser will be installed to properly mix the concentrate with ocean water. An NPDES Permit will be required for this discharge. **Table 7.1** is a summary of plant flow rates.

TABLE 7.1								
Town of Edisto Beach								
	Summary of RO Plant Flow Rates (gpm)							
	Raw	Feed	Blend	Permeate	Finished	Concentrate		
Skid #1	506.67	426.67	80.00	320.03	400.03	106.64		
Skid #2	506.67	426.67	80.00	320.03	400.03	106.64		
Skid #3	506.67	426.67	80.00	320.03	400.03	106.64		
Total	1520	1280	240	960	1200	320		

A 24-hour pump test was conducted on existing Well #6 during November 2016 and samples were collected for lab analysis. Lab analysis of the existing groundwater supply is included as **Appendix A**. High levels of chloride, sodium, bicarbonate alkalinity, and total dissolved solids were reported in this raw groundwater sample. All of these parameters are, of course, secondary standards, but to achieve the Town's goal of improved water quality, the RO plant will be designed to reduce these to acceptable levels.

Harn R/O Systems, Inc. prepared a computer analysis to predict finished water quality based upon their specific design of an RO treatment system. The design includes a 20% blend of raw water with permeate from the RO units as requested by the Town. Town officials conducted a "taste test" of water from their existing RO dispensing station at Town Hall that was blended with well water from the distribution system in ratios of 10% and 20%. The 20% blend was selected by the Town which will provide more treatment capacity with the same treatment units and it will still meet Town water quality goals and will comply with primary and secondary water standards. The computer analysis of the selected RO system is included as **Appendix B** and a summary of the water quality is shown in Table 7.2 below:

TABLE 7.2Town of Edisto BeachWater Quality Projections							
Parameter	Raw (mg/l)	Permeate (mg/l)	Blended (mg/l)				
Bicarbon. Alkalinity	519	25.75	126.06				
Sodium	512	18.14	123.52				
Chloride	490	12.8	108.24				
Fluoride	2.56	0.12	0.61				
рН	8.9	8.3	8.92				
TDS	1680	64.64	396.71				

Raw water quality based upon testing from well #6 sample collected November 2015

An emergency generator will be located on the same level as the treatment plant operations floor but outside the building. The generator will be sized to provide sufficient power for a minimum plant operating capacity of ½ PDD (480 gpm) during power outages. The generator fuel tank will be double-walled and self-contained located under the generator. The motor control center will be located in a separate room within the building. The plant building will also include a control room where the SCADA control system will be located and a separate room will contain the HSP system.

**Figure 7.1** is a conceptual layout of the operating floor while **Figure 7.2** shows an elevation view of the proposed treatment facility including the clearwell. **Figure 7.3** is a site plan of the proposed plant and proposed new well #7. The facility construction will comply with state and local codes and regulations.



February, 2017

Figure 7.1

**RO Treatment Plant** 

Floor Plan





A RO PLANT – UPPER LEVEL LAYO  

$$(G. 7.1)$$
  $1/4$  "=1'-0"

February, 2017

Figure 7.2

**RO Treatment Plant** 

**Elevation Section** 





February, 2017

Figure 7.3

RO Treatment Plant & Well #7

Site Plan





### 8. <u>STORAGE</u>

The clearwell, located under the treatment facility, discussed above, will cover an area of approximately 3,518 square feet (SF) and will contain 290,000 gallons at an 11-foot water depth. The clearwell is designed to provide in excess of the required 30-minute chlorine detention time and to allow for more continuous operation of the RO plant. The clearwell will be vented through the operations room floor (clearwell ceiling) and through the plant building wall to the exterior of the building. The top of the clearwell will be 2 feet above the 100-year flood elevation. Finished water in the clearwell will be discharged into the distribution system with the HSPs as previously described. A water level transducer within the clearwell will control the operation of the RO plant and supply wells.

The existing 200,000-gallon GST at Edisto State Park will be available for use during peak demand periods. As described previously, the GST will be used to store treated water only and the existing wells that now fill this tank will be taken offline. An automatic control valve (ACV) will be installed on a new line to be constructed between the GST and the existing 10-inch discharge line from the booster pumps that delivers water to the distribution system. The valve will open to fill the tank with treated water from the distribution system only during periods of lower demand during peak demand days (approximately 11:00 pm – 4:00 am). The ACV will be closed at all other times allowing the booster pumps to deliver stored water from the GST to the system upon demand.

The existing 100,000-gallon elevated storage tank will remain in service and the level in the tank will continue to provide the signal for the operation of water supply to the distribution system. Tank level now controls the operation of the wells but will control the operation of the HSP's after these improvements are completed. An ACV will be installed on the line feeding this tank. This ACV will close when the ACV at the GST is open and will reopen when the GST ACV closes.

### 9. <u>CONTROL SYSTEM</u>

A new supervisory control and data acquisition (SCADA) system will be installed to automatically control the operation of the water system. The existing system is now controlled by an antiquated proprietary SCADA system that requires replacement. The new SCADA system will receive data transmission from the remote locations through RF signals. The control center will be located in the control room at the water treatment facility. The Process & Instrumentation Diagram (P&ID) is included as **Figure 9.1**. This diagram graphically illustrates the control system for the improved water system. The P&ID specifically for the proposed RO system is also included as **Figure 9.1**. Figure 9.2, Process Flow Diagram, is a representation of the proposed improvements and existing infrastructure that will be included in the completed project and it depicts the flow of water through the various processes.



Basically, the level in the existing elevated tank will control the operation of the HSPs and the water level in the clearwell will control the operation of the water supply wells and, in turn, the operation of the RO plant. It is anticipated that there may be at least 3 different modes of operation depending upon seasonal demands. Since the improved water system is designed to meet PDD during the tourist season, treated water may become aged during the winter months unless operational changes are made. The SCADA system will allow those changes to be easily made on the touch-screen monitor. The 3-skid RO plant provides the flexibility to run only one skid during the winter months of low demand, 2 skids during average demand, or all 3 skids during peak demand months. The RO units should be run as continuously as possible and this arrangement will allow for the rotation of the skids on a daily basis during periods of lower demand increasing efficiency and allowing for maintenance of the idle skids. **Chart 9.2** shows actual system water use during 2015. The significant increase in water use during the summer months demonstrates the need for flexibility of the facility control system.



The GST may only be needed during periods of peak demand. The control system can be adjusted to allow the tank to fill during early morning hours of peak demand days and pump into the system during peak demand hours that same day as described previously.



February, 2017

Figure 9.1

Process & Instrumentation Diagram







LEGEND			ABBREVIATIONS		EQUIPMENT PREFIXES
	PROPOSED	BP CACL2 CL DIP DW FT	BACKFLOW PREVENTER CALCIUM CHLORIDE CHLORINE DUCTILE IRON PIPE DEEP WELL FLOW TRANSMITTER	FAL FC FCV FE FI FIR	FLOW ALARM FLOW CONTROLLER FLOW CONTROL VALVE (MODULATING) FLOW SENSOR FLOW INDICATOR FLOW INDICATOR RECORDER
$\bowtie$	NEW GATE VALVE	HSP L	HIGH SERVICE PUMP LEVEL	FIT FIQ	FLOW INDICATOR TRANSMITTER FLOW INDICATOR TOTAL
	NEW CHECK VALVE	M MBFV NAOCL	MOTOR MOTORIZED BUTTERFLY VALVE SODIUM HYPOCHLORITE	FT LAH LAL	LEVEL ALARM HIGH LEVEL ALARM LOW
M	MOTORORIZED BUTTERFLY VALVE	NC NO O.C. RO VED	NORMALLY CLOSED NORMALLY OPEN OPEN/CLOSE REVERSE OSMOSIS VARIABLE FREQUENCY DRIVE (VARIABLE SPEED)	LE LIR LIT LS	LEVEL SENSOR LEVEL INDICATOR RECORDER LEVEL INDICATOR TRANSMITTER LEVEL SWITCH LEVEL SWITCH LOW
<b>لا</b>	NEW LEVEL SENSOR	VI D		LSH LT PG PI	LEVEL SWITCH HIGH LEVEL TRANSMITTER PRESSURE GAUGE PRESSURE INDICATOR
0000	NEW VERTICAL TURBINE PUMP			PSH ZC ZIC ZO ZSC	PRESSURE SENSOR HIGH VALVE MOTOR CLOSED
Ç	SUBMERSIBLE PUMP			ZSO	VALVE MOTOR OPERATOR OPEN SWITCH
	NEW FLOW METER (MAGNETIC)				





TOTAL FLOW



### Process and Instrumentation Diagram Legend

NOTE: ALL FITTINGS TO BE STANDARD DIMENSIONS UNLESS OTHERWISE NOTED.

#### PROCESS DEVICE SYMBOLS GENERAL INSTRUMENT SYMBOLS INSTRUMENT LINE SYMBOLS ₩ "Y" STRAINER FIELD MOUNTED INSTRUMENT ----- MAJOR PROCESS PIPING OR FLOW CHANNEL VALVE: GATE, OR OTHER ----- OTHER PIPING PANEL MOUNTED INSTRUMENT VALVE: GLOBE DIAPHRAGM SEAL ------ FUTURE/PIPING BY OTHERS PANEL MOUNTED PILOT LIGHT VALVE: THREE WAY DRAIN ----- ELECTRIC SIGNAL └╲│ VALVE: BUTTERFLY, DAMPER OR LOUVER $\bigcap$ SHARED FIELD MOUNTED INSTRUMENT ------ PNEUMATIC SIGNAL PROPORTIONING OR O VALVE: ROTARY BALL TYPE METERING PUMP ----- ELECTRICAL DIRECTION ARROW $\ominus$ SHARED PANEL MOUNTED INSTRUMENT USE VALVE: DIAPHRAGM VOL ----- ELECTRICAL CONNECTION POINT VARIABLE AREA FLOW METER FIELD MOUNTED INSTRUMENT (COMPUTER FUNCTION) VALVE: GENERIC CHECK ----- FLOW DIRECTION ARROW FOR PIPING G use VALVE: CHECK ← PANEL MOUNTED INSTRUMENT (COMPUTER FUNCTION ----- PANEL VALVE: BALL CHECK -MAGNETIC FLOW METER $\bigtriangledown$ SHARED FIELD MOUNTED INSTRUMENT (PLC CONTROL) I (EL K- VALVE: DOUBLE DOOR CHECK $\bigotimes$ J K <sup>™s</sup> L SHARED PANEL MOUNTED INSTRUMENT (PLC CONTROL) $|\nabla|$ VALVE: PLUG TYPE INTERNAL SYSTEM SIGNAL LINK VALVE: FLOAT (SOFTWARE OR DATA LINK) $\bigcirc$ INSTRUMENTS SHARING COMMON HOUSING -X-FLUME FLOW METER TP ♦ UNDEFINED INTERLOCK LOGIC -> VENT TO ATMOSPHERE FILLED TRIANGLE INDICATES EQUIPMENT SUPPLIED UNDER THIS CONTRACT. ULTRASONIC FLOW METER N use AIR/VACUUM VALVE RELEASE 0 USE ✓ CHEMICAL INJECTOR Ŕ ANTI-SIPHON VALVE ERT (ENERGY RECOVERY TURBINE) AIR RELEASE VALVE FUNCTION DESIGNATIONS T TEI U MUI V V EXPANSION JOINT 5 WAY VALVE HIGH PRESSURE PUMP VACUUM BREAKER HAND SWITCH MODIFIERS INSTRUMENT MODIFIERS W WEIGH X UN CENTRIFUGAL PUMP Y EV $\Sigma$ ADD OR SUM (ADD AND SUBTRACT) HOA HAND OFF AUTO STATIC MIXER $\triangle$ SUBTRACT (DIFFERENCE) OAC OPEN AUTO CLOSE OBSERVATION POINT- ACRYLIC PIPE ✓ EXTRACT SQUARE ROOT LR LOCAL REMOTE L MIXER HACK FLOW PREVENTER ÷ DIVIDE OC OPEN-CLOSE - 🕺 PRESSURE RELIEF VALVE / INTEGRATE (TIME INTEGRAL) 00 ON-OFF PLATE HEAT EXCHANGER CI2 CHLORINE OOR ON-OFF-REMOTE CO2 CARBON DIOXIDE OSC OPEN-STOP-CLOSE COND CONDUCTIVITY TBR TOP-BOTTOM-REMOTE VALVE AND ACTUATOR SYMBOLS DO DISSOLVED OXYGEN TRANSDUCER & CONVERTER DESIGNATION pH <mark>pH</mark> DIAPHRAGM ACTUATOR S SOLENOID (AIR TO CLOSE) TURB TURBIDITY F VOLTAGE MCC MOTOR CONTROL CENTER FSK FREQUENCY SHIFT KEYING DIAPHRAGM ACTUATOR 5A ELECTRO-HYDRAULIC OPERATOR P (AIR TO OPEN) H HYDRAULIC | CURRENT DIAPHRAGM ACTUATOR Μ ELECTRIC MOTOR **-**(AIR TO AIR OR DOUBLE ACTING) NOTE: P PNEUMATIC THE P & ID SYMBOLS etc. PD PULSE DURATION 4 PRESSURE-REDUCING VALVE, Н ARE BASED ON THE INSTRUMENT HYDRAULIC CYLINDER SELF-CONTAINED SOCIETY OF AMERICA (ISA), PF PULSE FREQUENCY STANDARD ANSI/ISA-S5.1 (1984) BACK PRESSURE VALVE, R RESISTANCE (ELECTRICAL) 日式 AIR ACTUATOR SELF-CONTAINED (DOUBLE ACTING) - F AIR ACTUATOR - DIAPHRAGM VALVE (SPRING TO CLOSE) **PROPRIETARY INFORMATION!** THREE - WAY SOLENOID -2 AIR ACTUATOR This information is provided for the use of the Owner and the VALVE (SPRING TO OPEN) Engineer on this specific project - for bid evaluation and

This information is provided for the use of the Owner and the Engineer on this specific project – for bid evaluation and execution by Harn R/O Systems, Inc. The Owner and Engineer shall maintain the information in confidence. All proprietary information is the property of Harn R/O Systems, Inc. and shall be returned to Harn R/O Systems, Inc. or destroyed if the project is not executed by Harn R/O Systems, Inc.

## PRELIMINARY

VERIFY SCALES, SHOP SUPERVISOR

RELIMINARY

FOUR VALVE

FOUR - WAY SOLENOID

DATE

:	SS	#	DESCRIPTIONS	DATE	DRN REI		DB NO:	15-2100C 09/30/16	JOB:
	SIO		PKELIMINANT	09/30/16	UFS		ESIGN BY:	DFS	DRAWING TITLE:
	EVI	ł				(941)488-9671	CALE:	NTS	Process
	RI					SYSTEMS INC.	HECKED BY: PPROVED BY:		

#### **IDENTIFICATION LETTERS**

FIRST	LETTER	SUC	CEEDING LETTE	IRS
ASURED OR NITIATING VARIABLE	MODIFIER	READOUT OR PASSIVE FUNCTION	OUTPUT FUNCTION	MODIFIER
NALYSIS		ALARM		
BURNER, MBUSTION		USER'S CHOICE	USER'S CHOICE	USER'S CHOICE
NDUCTIVITY LECTRICAL)			CONTROL	
ER'D CHOICE	DIFFERENTIAL			
TAGE (EMF)		PRIMARY ELEMENT		
LOW RATE	RATIO (FRACTION)			
R'S CHOICE		GLASS		
) (MANUALLY NITIATED)				HIGH
CURRENT LECTRICAL)		INDICATE		
POWER	SCAN			
E OR TIME- SCHEDULE	TIME RATE OF CHANGE		CONTROL STATION	
LEVEL		LIGHT (PILOT)		LOW
NISTURE OR HUMIDITY	MOMENTARY			MIDDLE OR INTER- MEDIATE
R'S CHOICE		USER'S CHOICE	USER'S CHOICE	USER'S CHOICE
R'S CHOICE		ORIFICE (RESTRICTION)		
ESSURE OR VACUUM		POINT (TEST CONNECTION)		
QUANTITY	INTEGRATE OR TOTALIZE	INTEGRATE OR TOTALIZE		
RADIATION		RECORD OR PRINT		
SPEED OR REQUENCY	SAFETY		SWITCH	
MPERATURE			TRANSMIT	
TIVARIABLE		MULTIFUNCTION	MULTIFUNCTION	MULTIFUNCTION
/IBRATION			VALVE, DAMPER, OR LOUVER	
HT OR FORCE		WELL		
CLASSIFIED		UNCLASSIFIED	UNCLASSIFIED	UNCLASSIFIED
NT, STATE, PRESENCE			RELAY OR COMPUTE	
POSITION, DIMENSION			DRIVE, ACTUATOR OR UNCLASSIFIED FINAL CONTROL ELEMENT	

### COMPUTER SYSTEMS INTERFACE SYMBOLS

NOTE: REFER TO DETAILED SYSTEM SPECIFICATIONS FOR FUNCTIONAL DESCRIPTION. ALSO SEE I/O SCHEDULES FOR COMPLETE INPUT AND OUTPUT LISTINGS.

> COMPUTER OR DISTRIBUTED CONTROL SYSTEM FUNCTION BLOCK

PROGRAMMABLE LOGIC CONTROLLER SYSTEM FUNCTION BLOCK

CONTROL ALGORITHM IN SPECIFICATIONS

DIGITAL SYSTEM I/O INTERFACE DIRECTION OF ARROW DENOTES WHETHER INPUT OR OUTPUT. FILLED ARROW INDICATES DIGITAL SIGNAL.

LETTER, TAG NUMBER, ABBREVIATIONS AND OTHER ANNOTATIONS ARE SIMILAR TO THE GENERAL INSTRUMENT LEGEND. SOLID LINE REPRESENTS SHARED DISPLAY OR OPERATOR ACCESSIBLE FUNCTION.

DENOTES MULTIPLE I/O POINTS W/ (n) AS THE NUMBER OF POINTS

TOWN OF EDISTO BEACH	DRAWING NO.
WATER SYSTEM IMPROVEMENT PROJECT	SUB ASSEMBLY PAGE NO.
w me: Process and Instrumentation Diagram I agond	1 of 3
Tocess and instrumentation Diagram Legend	DRAWING SET PAGE NO.



February, 2017

Figure 9.2

Process Flow Diagram





NO. OF TRAINS ON	REQUIRED RAW WATER FLOW (gpm)	RO FEED FLOW (gpm)	BLENDED PRODUCT (gpm)	CONCENTRATE FLOW (gpm)
Ι	507	427	400	107
2	1014	854	800	214
3	1521	1281	1200	321

### 10. <u>HYDRAULIC MODEL</u>

A computerized hydraulic model of the entire water system developed during previous engineering studies was updated for recent infrastructure improvements and current operating data. Data for proposed improvements was entered into the model for each of the 8 options considered during the matrix development process. This data included but was not limited to:

- Supply wells pressure and flow rates.
- RO plant treatment capacity.
- HSPs pressure and flow rates.
- Clearwell volume per foot of depth.
- Elevated storage tank volume per foot of depth and corresponding elevations.
- ASR pressure and flow rate.
- GST volume per foot of depth.
- GST booster pumps pressure and flow rates.
- PDD and fire flow within the water distribution system.

The model was manipulated with various control points for pumps, RO plant, ASR and tank elevations to provide sizing for each proposed improvement option required to meet PDD with a fire flow of 1,000 gpm for 2 hours impressed during PHD. PHD peaking factor of 2.1 X PDD was used to be conservative since AWWA average PHD factor is 1.8 X PDD. Many options failed to meet the required conditions and were eliminated from consideration. The options that did meet the required conditions were compared on an initial cost and a life cycle basis.

**Figure 10.1** is a graph of the model results for selected Option 4C. It shows tank levels and pumping rates for existing infrastructure and the new improvements included with this option during PDD with 1,000 gpm fire flow for 2 hours during the peak hour. Even though it is highly unlikely that this scenario will ever occur, the modeling results indicate that Option 4C will be capable of meeting this demand provided all infrastructure is operating properly.

February, 2017

Figure 10.1

Hydraulic Modeling Graph

Option 4C





EDISTO BEACH PROPOSED RO PLANT **OPTION 4C** 

PMP-CW-1A - Option 4C (72 Hour) - 1,200 gpm RO, 3518 SF clearwell, 1,000 GPM FF at J-28 from 8-10 AM on Day 2 - Flow (Total) PMP-CW-1B - Option 4C (72 Hour) - 1,200 gpm RO, 3518 SF clearwell, 1,000 GPM FF at J-28 from 8-10 AM on Day 2 - Flow (Total) \_... PMP-CW-2 - Option 4C (72 Hour) - 1,200 gpm RO, 3518 SF clearwell, 1,000 GPM FF at J-28 from 8-10 AM on Day 2 - Flow (Total) GST Booster Pump-2 - Option 4C (72 Hour) - 1,200 gpm RO, 3518 SF clearwell, 1,000 GPM FF at J-28 from 8-10 AM on Day 2 - Flow (Tota Elevated Tank - Option 4C (72 Hour) - 1,200 gpm RO, 3518 SF clearwell, 1,000 GPM FF at J-28 from 8-10 AM on Day 2 - Level (Calculated) T-CW-1 - Option 4C (72 Hour) - 1,200 gpm RO, 3518 SF clearwell, 1,000 GPM FF at J-28 from 8-10 AM on Day 2 - Level (Calculated) Ground Tank 1 - Option 4C (72 Hour) - 1,200 qpm RO, 3518 SF clearwell, 1,000 GPM FF at J-28 from 8-10 AM on Day 2 - Level (Calculated)

FIGURE 10.1

### 11. <u>SUMMARY</u>

The proposed water system improvements for the Town of Edisto Beach will be constructed under a Progressive Design/Build delivery method. Permitting for this project is scheduled to be completed during 2017 with construction beginning immediately after all permits are issued with completion anticipated within 12-14 months.

Improvements included in this project consist of:

- Two new 10-inch Santee wells approximately 580-feet deep with submersible pumps and VFD motors.
- Approximately 10,000 feet of new transmission water main to connect wells to the treatment plant.
- Water treatment plant consisting of 3 RO treatment skids each with a permeate capacity of 320 gpm for a combined treatment capacity of 1,200 gpm including a 20% blend with raw well water. The plant will also include pre and post treatment equipment and a system to chemically clean the RO membranes.
- Water treatment plant building housing RO treatment system, chemical systems, motor control center, emergency generator, high service pumps, control room/SCADA and rest room.
- Approximately 1,900 feet of concentrate discharge line with length dependent upon required depth of diffuser from ocean surface.
- Reinforced concrete clearwell will be constructed under the treatment plant building. The surface area of the clearwell will be approximately 3,518 SF with an 11-foot water depth and 2 feet of freeboard. Total volume of the clearwell will be 290,000 gallons.
- Three vertical turbine high service pumps with VFD motors. One pump rated at 1,200 gpm and the other two rated at 600 gpm each.
- Automatic control valves will be installed on the fill line of both the existing elevated storage tank and GST. New SCADA controls will allow the GST to fill during off-peak hours on high demand days, and deliver stored water from the GST to the system as needed during peak hours. Control valve on the elevated tank will be closed while the GST is filling.

Summary of completed project capacities:

- Current ADD 587,500 gpd
- Design ADD 705,000 gpd
- Design PDD 1,621,500 gpd (1,126 gpm)



•	Total well supply	1,521 gpm + 385 gpm Reserve
•	Blended RO	1,728,000 gpd (1,200 gpm)
•	High Service Pumps	1,200 gpm, 600 gpm, 600 gpm
•	Clearwell Capacity	290,000 gallons
•	Existing Storage	ET=100,000 gal., GST=200,000 gal,



February, 2017

Appendix A

Lab Analysis-Existing Well #6





9104 Canvas Lane ∴ Ladson, South Carolina 29456 Telephone (843) 871-4999 △ Fax (843) 875-2266 e-mail: tls@tridentlabs.com

### **REPORT OF ANALYSIS**

Thomas & Hutton Engineering 935 Houston Northcutt Blvd. Mt. Pleasant, SC 29465 Attn: Mark Yodice

Report Date: 01/05/16

Sampled: 11/20/15 10:29 Received: 11/20/15 11:40 Sample Id: 0154218 Collected By: JGL Received By: KDL Sample Number(s): 190427 - 190430 Sample Matrix: DW Project Name: Edisto Beach 1 of 3 Location: Well 6 **ANALYSIS METHOD RESULT UNITS** DATE/TIME ANALYST Sample Type: Grab **Bicarbonate Alkalinity** SM 2320B 519 11/23/15 10:00 mg/l LJH Carbonate Alkalinity SM 2320B 0 mg/l 11/23/15 10:00 LJH Chloride EPA 300.0 490 mg/l 11/20/15 15:33 MBL Fluoride EPA 300.0 2.56 mg/l 11/20/15 13:38 MBL Nitrate-Nitrogen EPA 300.0 < 0.5 mg/l 11/20/15 13:38 MBL Residue, Filterable (TDS) 1398 SM 2540C mg/l 11/25/15 12:00 ACE Specific Conductance EPA 120.1 2.61 mS/cm 11/20/15 14:00 ACE Sulfate EPA 300.0 52.8 mg/l 11/20/15 13:43 MBL Metals Prep EPA 200.2 Complete None 11/24/15 08:00 MBL Barium EPA 200.7 < 0.050 mg/l 11/25/15 10:46 MBL Calcium EPA 200.7 5.3 mg/l 11/25/15 10:46 MBL Chromium EPA 200.7 0.005 mg/l 11/25/15 10:46 MBL Copper EPA 200.7 0.105 mg/l 11/25/15 10:46 MBL Iron EPA 200.7 < 0.3 mg/l 11/25/15 10:46 MBL Manganese EPA 200.7 < 0.010 mg/l 11/25/15 10:46 MBL Zinc EPA 200.7 0.089 11/25/15 10:46 mg/l MBL Aluminum EPA 200.7 < 0.050 mg/l 11/25/15 10:46 MBL Sub Work Sub Contractor Attached None 12/04/15 14:16 JL

FIELD SERVICES I.D. NO 08566

0

REPORT APPROVED BY:

LABORATORY I.D. NO. 10122.

Report Comments :

Ammended Report: Incorrect Result entered.



9104 Canvas Lane △ Ladson, South Carolina 29456 Telephone (843) 871-4999 △ Fax (843) 875-2266 e-mail: tls@tridentlabs.com

### **QC SUMMARY**

1/5/16

Sample ID: 0154218

Report Date:

Thomas & Hutton Engineering							
935 Houston Northcutt Blvd.							
Mt. Pleasant, SC 29465							
Attn: Mark Yodice							

Batch	30113	Method :	EPA 300.0				
Parameter		Expected	Actual Result	% Rec	Range	Analyst	Date/Time
	LCS-CL Chloride	2	1.99	99.35	90 - 110	MBL	11/20/2015 1:42:34 PM
	LCS-F Fluoride	2	2.16	108.15	90 - 110	MBL	11/20/2015 1:42:34 PM
	LCS-NO3 Nitrate-Nitrogen	2	2.01	100.30	90 - 110	MBL	11/20/2015 1:42:34 PM
	LCS-SO4 Sulfate	2	2.12	106.05	90 - 110	MBL	11/20/2015 1:42:34 PM
	MSPK-F Fluoride	5	5.34	106.88	80 - 120	MBL	11/20/2015 1:42:34 PM
	MSPK-NO3 Nitrate-Nitrogen	5	4.84	96.72	80 - 120	MBL	11/20/2015 1:42:34 PM
	MSPK-CL Chloride	9.998	9.90	99.00	80 - 120	MBL	11/20/2015 1:42:34 PM
	MSPK-SO4 Sulfate	20.2	20.50	101.49	80 - 120	MBL	11/20/2015 1:42:34 PM
Batch	30115	Method :	EPA 120.1				
Paramete	ər	Expected	Actual Result	% Rec	Range	Analyst	Date/Time
	Duplicate	2.61	2.62	0.38	-10 - 10	MBL	11/20/2015 2:28:24 PM
	LCS Specific Conductance	1410	1416.00	100.43	90 - 110	MBL	11/20/2015 2:28:24 PM
Batch	30125	Method :	SM 2320B				
Paramete	r	Expected	Actual Result	% Rec	Range	Analyst	Date/Time
	Duplicate Bicarbonate Alkalinity	0	0.00	0.00	-10 - 10	LJH	11/23/2015 11:40:19 AM
Batch	30126	Method :	SM 2320B				
Paramete	r	Expected	Actual Result	% Rec	Range	Analyst	Date/Time
	Duplicate Carbonate Alkalinity	0	0.00	0.00	-10 - 10	LJH	11/23/2015 11:43:42 AM
Batch	30150	Method :	EPA 200.7				
Paramete	r	Expected	Actual Result	% Rec	Range	Analyst	Date/Time
	LCS-AL Aluminum	1	1.09	109.00	85 - 115	MBL	11/25/2015 8:04:34 AM
	LCS-BA Barium	1	1.09	109.00	85 - 115	MBL	11/25/2015 8:04:34 AM
	LCS-CA Calcium	1	1.11	111.00	85 - 115	MBL	11/25/2015 8:04:34 AM
	LCS-CR Chromium	1	1.06	106.00	85 - 115	MBL	11/25/2015 8:04:34 AM
	LCS-CU Copper	1	1.02	102.00	85 - 115	MBL	11/25/2015 8:04:34 AM
	LCS-FE Iron	1	1.24	124.00	85 - 115	MBL	11/25/2015 8:04:34 AM

LABORATORY I.D. NO. 10122, FIELD SERVICES I.D. NO 08566 REPORT APPROVED BY:

**Report Comments :** 

Ammended Report: Incorrect Result entered.



9104 Canvas Lane ∠\ Ladson, South Carolina 29456 Telephone (843) 871-4999 △ Fax (843) 875-2266 e-mail: tls@tridentlabs.com

### **QC SUMMARY**

Thomas & Hutton Engineering						
935 Houston Northcutt Blvd.	Report I	Date: 1/5/16	Samp	Sample ID: 0154218		
Mt. Pleasant, SC 29465						
Attn: Mark Yodice						
LCS-MN Manganese	1	1.07	107.00	85 - 115	MBL	11/25/2015 8:04:34 AM
LCS-ZN Zinc	1	1.07	107.00	85 - 115	MBL	11/25/2015 8:04:34 AM
MSPK-CR Chromium	1	1.10	110.00	75 - 125	MBL	11/25/2015 8:04:34 AM
MSPK-CU Copper	1	1.08	108.00	75 - 125	MBL	11/25/2015 8:04:34 AM
MSPK-MN Manganese	1	1.09	109.00	75 - 125	MBL	11/25/2015 8:04:34 AM
MSPK-ZN Zinc	1	1.23	123.00	75 - 125	MBL	11/25/2015 8:04:34 AM
Batch 30178	Method :	SM 2540C				
Parameter	Expected	Actual Result	% Rec	Range	Analyst	Date/Time
Duplicate Residue, Filterable (TDS)	1398	1490.00	6.58	-10 - 10	ACE	11/25/2015 12:00:00 PM

LABORATORY I.D. NO. 10122, FIELD SERVICES I.D. NO 08566 REPORT APPROVED BY:

Report Comments : Ammended Report: Incorrect Result entered.

## **Davis & Brown**

PO Box 15038 Quinby, SC 29506 (843) 665-6746 FAX: (843) 629-1444

## **Certificate of Analysis**

Client:	ACCESS ANALYTICAL	South Carolina Certification Number: 21117
	7478 CARLISLE ST	
	IRMO, SC 29063	
Contact:	ASHLEY AMICK	Presint Dutor 02 Dec 15
Client #:	941	Receipt Date: 02-Dec-15
		Report Date: 07-Jan-16
Samuela Datas	20.51 15	
Sample Date:	20-Nov-15	1. 7/. 1
SDC #·	SDC 100601	Approved By: Chan. Chand

Van Ward

Lab Director

 SDG #:
 SDG-109601
 Approved By:

 Lab Sample ID: LSID-242559
 190430
 Approved By:

		Reporting	2					
Parameter	Result	Limit	Unit	Method	Flag	Date	Time	Analyst
Beryllium, Total	<0.001	0.001	mg/Ĺ	EPA 200.7		12/16/2015	11:40	JR
Boron, Total	2.01	0.02	mg/L	EPA 200.7		12/17/2015	14:53	JR
Magnesium, Total	8.07	0.02	mg/L	EPA 200.7		12/4/2015	19:50	JR
Nickel, Total	< 0.005	0.005	mg/L	EPA 200.7		12/14/2015	13:28	JR
Potassium, Total	<25	25	mg/L	EPA 200.7		12/16/2015	9:07	JR
Sodium, Total	512	25	mg/L	EPA 200.7		12/16/2015	9:07	JR
Silver, Total	<0.005	0.005	mg/L	EPA 200.7 / 200.		12/15/2015	15:31	JR/AE
Mercury, Total	<0.20	0.2	ug/L	EPA 245.1		12/3/2015	9:00	CG
Thallium, Total	<0.5	0.5	ug/L	EPA 279.2/ 200.		12/16/2015	13:19	JR
Lead, Total	0.001	0.001	mg/L	SM 3113B-2010		1/5/2016	12:00	JR
Arsenic, Total	<0.005	0.005	mg/L	SM 3113B-99		1/5/2016	16:27	JR
Cadmium, Total-PQL	0.0001	0.0001	mg/L	SM 3113B-99		1/6/2016	10:21	JR
Selenium, Total	<0.005	0.005	mg/L	SM 3113B-99		1/6/2016	10:04	JR

Revision 2

Page 1

February, 2017

Appendix **B** 

Reverse Osmosis System Analysis



Case: 5

9/25/2016

ROSA 9.1 ConfigDB u399339 356

Reverse Osmosis System Analysis for FILMTEC<sup>™</sup> Membranes Project: Santee Well 6 WQ Town Hall Cases JEN, Harn R/O Systems, Inc.

Project Information: Edisto Beach

Case-specific: three 320 gpm perrm. skids

### System Details

Feed Flow to Stage 1		4	426.67 gpm F		Pass 1	Pass 1 Permeate Flow		320.01 gpm		Osmotic Pressure:			
Raw '	Water Flow to System	5	506.67	gpm	Pass 1	Recovery		75.00 %			Feed	16.50 ps	sig
Feed	Pressure	1	10.32	psig 2	Feed T	emperatur	re	25.0 C		С	oncentrate	62.46 ps	sig
Flow	Factor		0.85	5	Feed T	DS		1724.21 mg/l		Average		39.48 ps	sig
Chem	m. Dose (100% H2SO4) 0.00 Number of Elements 84 Average NDP		NDP	71.13 psig									
Total Active Area		336	500.00	) ft <sup>2</sup>	Average Pass 1 Flux			13.71 gfd		Power			W
Water	r Classification: Well W	/ater S	SDI <	3	Bypas	s Blending	; Flow	80.00 gpr	n	Specific	Energy	1.20 kV	Wh/kgal
Syste	m Recovery		78.95	5 %	Total I	Blended Pr	roduct	400.01 gpr	n				
				Feed	Feed	Recirc	Conc	Conc	Perm	Avg	Perm	Boost	Perm
Stage	Element	#PV	#Ele	Flow	Press	Flow	Flow	Press	Flow	Flux	Press	Press	TDS
				(gpm)	(psig)	(gpm)	(gpm)	(psig)	(gpm)	(gfd)	(psig)	(psig)	(mg/l)
1	BW30XFRLE-400/34	8	7	426.67	105.32	0.00	201.51	92.95	225.15	14.47	0.00	0.00	38.20
2	BW30XFRLE-400/34	4	7	201.51	117.95	0.00	106.65	106.18	94.86	12.20	0.00	30.00	107.06

Pass Streams (mg/l as Ion)										
Nomo	Food	A divisted Food	Conce	entrate	Permeate					
Iname	гееа	Adjusted Feed	Stage 1	Stage 2	Stage 1	Stage 2	Total	Blended Total		
NH4+ + NH3	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
K	18.08	18.08	37.69	69.92	0.52	1.46	0.80	4.25		
Na	534.86	538.90	1128.03	2102.27	11.61	32.68	17.85	122.06		
Mg	6.16	6.16	13.00	24.48	0.04	0.10	0.05	1.28		
Ca	4.62	4.62	9.75	18.36	0.03	0.07	0.04	0.96		
Sr	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
Ba	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
CO3	10.01	10.01	27.59	62.76	0.00	0.02	0.01	0.41		
HCO3	586.49	586.49	1209.68	2221.57	17.19	47.75	26.25	141.52		
NO3	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
Cl	474.00	474.00	994.54	1858.57	8.11	23.08	12.55	104.84		
F	3.30	3.30	6.87	12.72	0.10	0.29	0.16	0.79		
SO4	55.15	55.15	116.35	218.89	0.38	1.07	0.58	11.50		
SiO2	27.48	27.48	57.93	108.99	0.23	0.53	0.32	5.75		
Boron	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
CO2	4.28	4.28	8.02	14.79	5.06	9.11	6.26	4.71		
TDS	1720.18	1724.21	3601.47	6698.55	38.20	107.06	58.61	393.35		
pH	8.20	8.20	8.19	8.14	6.73	6.89	6.81	7.61		

\*Permeate Flux reported by ROSA is calculated based on ACTIVE membrane area. DISCLAIMER: NO WARRANTY, EXPRESSED OR IMPLIED, AND NO WARRANTY OF MERCHANTABILITY OR FITNESS FOR A PARTICULAR PURPOSE, IS GIVEN. Neither FilmTec Corporation nor The Dow Chemical Company assume any obligation or liability for results obtained or damages incurred from the application of this information. Because use conditions and applicable laws may differ from one location to another and may change with time, customer is responsible for determining whether products are appropriate for customer's use. FilmTec Corporation and The Dow Chemical Company assume no liability, if, as a result of customer's use of the ROSA membrane design software, the customer should be sued for alleged infringement of any patent not owned or controlled by the FilmTec Corporation nor The Dow Chemical Company.

### **Design Warnings**

-None-

### **Solubility Warnings**

Langelier Saturation Index > 0 Stiff & Davis Stability Index > 0

CaF2 (% Saturation) > 100%

Antiscalants may be required. Consult your antiscalant manufacturer for dosing and maximum allowable system recovery.

#### **Stage Details**

Stage 1	Stage 1 Element Recovery		Perm Flow	Perm TDS	Feed Flow	Feed TDS	Feed Press
Stage 1			(gpm)	(mg/l)	(gpm)	(mg/l)	(psig)
	1	0.09	4.73	21.84	53.33	1724.21	105.32
	2	0.09	4.48	25.75	48.61	1889.39	102.76
	3	0.10	4.24	30.55	44.13	2077.99	100.51
	4	0.10	4.01	36.52	39.89	2294.93	98.53
	5	0.11	3.79	44.07	35.88	2546.61	96.81
	6	0.11	3.57	53.77	32.10	2841.03	95.32
	7	0.12	3.34	66.51	28.53	3188.47	94.04
Stage 2 Element Recovery							
Stage 2	Element I	Recovery	Perm Flow (gpm)	Perm TDS (mg/l)	Feed Flow (gpm)	Feed TDS (mg/l)	Feed Press (psig)
Stage 2	Element H	Recovery 0.09	Perm Flow (gpm) 4.53	Perm TDS (mg/l) 57.00	Feed Flow (gpm) 50.38	Feed TDS (mg/l) 3601.47	Feed Press (psig) 117.95
Stage 2	Element H 1 2	Recovery 0.09 0.09	Perm Flow (gpm) 4.53 4.17	Perm TDS (mg/l) 57.00 69.29	Feed Flow (gpm) 50.38 45.85	Feed TDS (mg/l) 3601.47 3951.00	Feed Press (psig) 117.95 115.58
Stage 2	Element F	Recovery 0.09 0.09 0.09	Perm Flow (gpm) 4.53 4.17 3.79	Perm TDS (mg/l) 57.00 69.29 85.11	Feed Flow (gpm) 50.38 45.85 41.68	Feed TDS (mg/l) 3601.47 3951.00 4338.14	Feed Press (psig) 117.95 115.58 113.49
Stage 2	Element F 1 2 3 4	Recovery 0.09 0.09 0.09 0.09	Perm Flow (gpm) 4.53 4.17 3.79 3.40	Perm TDS (mg/l) 57.00 69.29 85.11 105.64	Feed Flow (gpm) 50.38 45.85 41.68 37.89	Feed TDS (mg/l) 3601.47 3951.00 4338.14 4762.32	Feed Press (psig) 117.95 115.58 113.49 111.65
Stage 2	Element F 1 2 3 4 5	Recovery 0.09 0.09 0.09 0.09 0.09	Perm Flow (gpm) 4.53 4.17 3.79 3.40 3.00	Perm TDS (mg/l) 57.00 69.29 85.11 105.64 132.48	Feed Flow (gpm) 50.38 45.85 41.68 37.89 34.49	Feed TDS (mg/l) 3601.47 3951.00 4338.14 4762.32 5219.96	Feed Press (psig) 117.95 115.58 113.49 111.65 110.03
Stage 2	Element F 1 2 3 4 5 6	Recovery 0.09 0.09 0.09 0.09 0.09 0.09	Perm Flow (gpm) 4.53 4.17 3.79 3.40 3.00 2.60	Perm TDS (mg/l) 57.00 69.29 85.11 105.64 132.48 167.77	Feed Flow (gpm) 50.38 45.85 41.68 37.89 34.49 31.49	Feed TDS (mg/l) 3601.47 3951.00 4338.14 4762.32 5219.96 5703.56	Feed Press (psig) 117.95 115.58 113.49 111.65 110.03 108.59

Permeate Flux reported by ROSA is calculated based on ACTIVE membrane area. DISCLAIMER: NO WARRANTY, EXPRESSED OR IMPLIED, AND NO WARRANTY OF MERCHANTABILITY OR FITNESS FOR A PARTICULAR PURPOSE, IS GIVEN. Neither FilmTec Corporation nor The Dow Chemical Company assume any obligation or liability for results obtained or damages incurred from the application of this information. Because use conditions and applicable laws may differ from one location to another and may change with time, customer is responsible for determining whether products are appropriate for customer's use. FilmTec Corporation and The Dow Chemical Company assume no liability, if, as a result of customer's use of the ROSA membrane design software, the customer should be sued for alleged infringement of any patent not owned or controlled by the FilmTec Corporation nor The Dow Chemical Company.

### **ROSA** Detailed Report

### **Scaling Calculations**

	Raw Water	Adjusted Feed	Concentrate
pH	8.20	8.20	8.14
Langelier Saturation Index	0.00	0.00	1.08
Stiff & Davis Stability Index	0.29	0.29	0.85
Ionic Strength (Molal)	0.03	0.03	0.10
TDS (mg/l)	1720.18	1724.21	6698.55
HCO3	586.49	586.49	2221.57
CO2	4.28	4.28	14.79
CO3	10.01	10.01	62.76
CaSO4 (% Saturation)	0.05	0.05	0.35
BaSO4 (% Saturation)	0.00	0.00	0.00
SrSO4 (% Saturation)	0.00	0.00	0.00
CaF2 (% Saturation)	6.69	6.69	395.23
SiO2 (% Saturation)	17.82	17.82	73.45
Mg(OH)2 (% Saturation)	0.01	0.01	0.02

To balance: 4.03 mg/l Na added to feed.